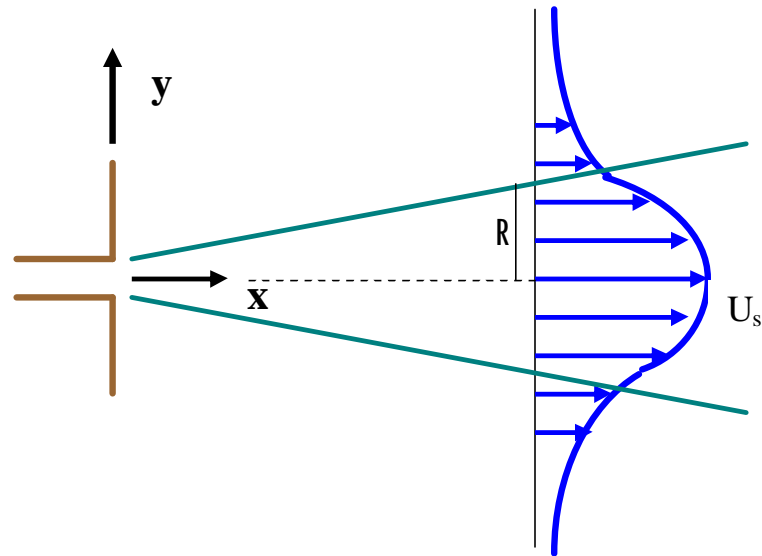


Turbulent Plane Jet Flow

Turbulent jet flow shown schematically in the figure is studied in this section.



Equation of Motion

$$U \frac{\partial U}{\partial x} + V \frac{\partial U}{\partial y} + \frac{\partial}{\partial y} \overline{u'v'} = 0 \quad (1)$$

Momentum Integral

$$\int_{-\infty}^{+\infty} dy \left[\frac{\partial}{\partial x} (U^2) + \frac{\partial}{\partial y} (UV) + \frac{\partial}{\partial y} \overline{u'v'} \right] = 0 \quad (2)$$

or

$$\frac{d}{dx} \int_{-\infty}^{+\infty} U^2 dy = 0. \quad (3)$$

Integrating Equation (3) we find

$$\rho \int_{-\infty}^{+\infty} U^2 dy = M = \text{Jet Momentum} \quad (4)$$

That is the total momentum of the jet is conserved.

Continuity Equation

$$\frac{\partial U}{\partial x} + \frac{\partial V}{\partial y} = 0 \quad (5)$$

Introducing the stream function, ψ ,

$$U = \frac{\partial \psi}{\partial y}, \quad V = -\frac{\partial \psi}{\partial x} \quad (6)$$

the continuity equation given by (5) is identically satisfied.

Self similar solutions for the mean velocity and turbulent stress are given as

$$U = U_s f(\xi), \quad -\overline{u'v'} = U_s^2 g(\xi), \quad \xi = \frac{y}{\ell} \quad (7)$$

We assume

$$U_s = c x^m, \quad \ell = D x^n. \quad (8)$$

Equation (1) then implies, $2m - 1 = 2m - n$, i.e. $n = 1$

Equation (4) implies. $2m + n = 0$, i.e. $m = -\frac{1}{2}$

Hence,

$$U_s = C x^{-\frac{1}{2}}, \quad \ell = D x. \quad (9)$$

Now,

$$\mathbf{x} = \frac{y}{\ell} = \frac{y}{Dx}, \quad \frac{\partial \mathbf{x}}{\partial x} = -\frac{y}{Dx^2} = -\frac{\mathbf{x}}{x}, \quad \frac{\partial \mathbf{x}}{\partial y} = \frac{1}{\ell} = \frac{1}{Dx} \quad (10)$$

Integrating (6), we find

$$\mathbf{y} = \ell U_s \int_0^{\mathbf{x}} f(\mathbf{x}_1) d\mathbf{x}_1 \quad (11)$$

Let

$$F(\xi) = \int_0^{\xi} f(\xi_1) d\xi_1 \quad (12)$$

Then,

$$\psi = CDx^{\frac{1}{2}}F(\xi) \quad (13)$$

$$-\overline{u'v'} = C^2x^{-1}g(\xi) \quad (14)$$

Now

$$V = -\frac{\partial\psi}{\partial x} = -CD \left[\frac{1}{2}x^{-\frac{1}{2}}F(\xi) + x^{\frac{1}{2}}F'(\xi) \left(-\frac{\xi}{x} \right) \right] = -CDx^{-\frac{1}{2}} \left(\frac{1}{2}F - \xi F' \right) \quad (15)$$

$$U = Cx^{-\frac{1}{2}}F'(\xi) \quad (14)$$

$$\frac{\partial U}{\partial x} = -\frac{1}{2}Cx^{-\frac{3}{2}}F' + cx^{-\frac{1}{2}}F'' \left(-\frac{\xi}{x} \right) = -Cx^{-\frac{3}{2}} \left(\frac{1}{2}F' + \xi F'' \right) \quad (15)$$

$$\frac{\partial U}{\partial y} = Cx^{-\frac{1}{2}}F''(\xi) \frac{1}{Dx} = \frac{C}{D}x^{-\frac{3}{2}}F'' \quad (16)$$

$$-\frac{\partial \overline{u'v'}}{\partial y} = \frac{C^2}{D}x^{-2}g' \quad (17)$$

Using (13) – (17), Equation (1) becomes

$$-Cx^{-\frac{1}{2}}F' \left(-Cx^{-\frac{3}{2}} \left(\frac{1}{2}F' + \xi F'' \right) \right) - CDx^{-\frac{1}{2}} \left(\frac{1}{2}F - \xi F' \right) \frac{C}{D}x^{-\frac{3}{2}}F'' = \frac{C^2}{D}x^{-2}g'. \quad (18)$$

Simplifying (18), it follows that

$$-F' \left(\frac{1}{2}F' + \xi F'' \right) - \left(\frac{1}{2}F - \xi F' \right) F'' = \frac{1}{D}g' \quad (19)$$

or

$$F'^2 + FF'' = -\frac{2}{D}g' \quad (20)$$

Introducing the eddy viscosity,

$$-\overline{u'v'} = \nu_T \frac{\partial U}{\partial y} \quad (21)$$

or

$$\nu_T = -\frac{\overline{u'v'}}{\frac{\partial U}{\partial y}} = \frac{U_s^2 g(\xi)}{U_s \ell F''} = U_s \ell \frac{g}{F''} \quad (22)$$

That is

$$\frac{\nu_T}{U_s \ell} = \frac{1}{R_T} = \frac{g}{F''} \quad (23)$$

or

$$g = \frac{1}{R_T} F'', \quad R_T \approx 25.7 \quad (24)$$

Equation (20) now becomes

$$F'^2 + FF'' = -F''' \quad (25)$$

where we assumed $\frac{2}{DR_T} = 1$ and $D = 0.078$. Equation (25) may be restated as

$$(FF')' + F''' = 0. \quad (26)$$

Integrating Equation (26), we find

$$FF' + F'' = c_1 \quad (27)$$

Boundary conditions for the jet flow are

$$F'(0) = 1, F'(\infty) = 0, F(0) = 0, \text{ (or } F''(\infty) = 0 \text{)} \quad (28)$$

Hence, $c_1 = 0$, and integrating Equation (27), we find

$$\frac{1}{2}F^2 + F' = c_2 = 1 \text{ or } \frac{2dF}{2-F^2} = d\xi, \quad 2\frac{1}{\sqrt{2}} \tan^{-1} \frac{F}{\sqrt{2}} = \mathbf{x} + c_3, \quad c_3 = 0. \quad (29)$$

Therefore,

$$F = \sqrt{2} \tanh \frac{\xi}{\sqrt{2}}, \quad (30)$$

and

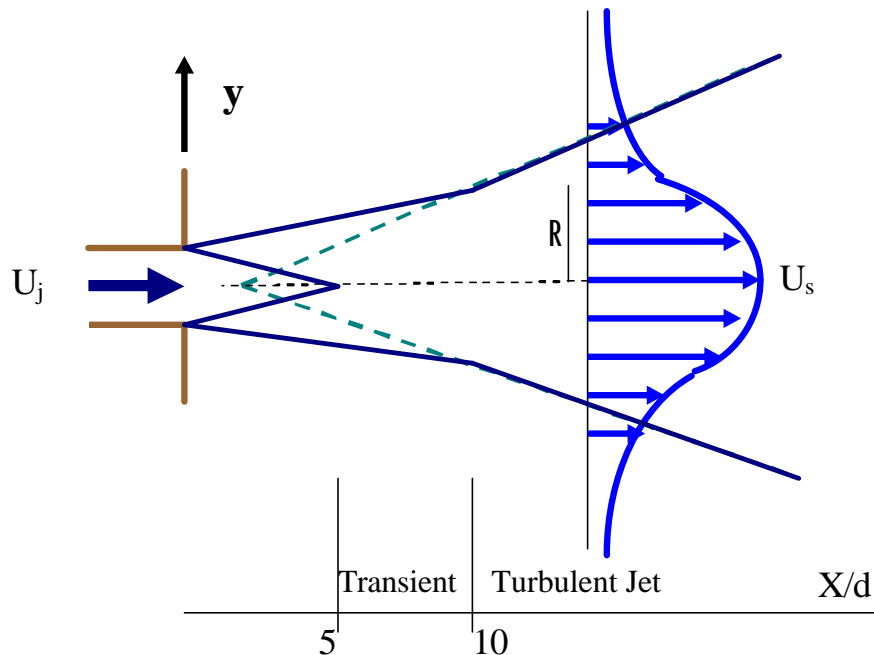
$$f = F' = \frac{1}{\cos^2 \frac{\xi}{\sqrt{2}}} = \operatorname{sech}^2 \frac{\xi}{\sqrt{2}} \quad (31)$$

If d is the width of the jet, then

$$\frac{U_s}{U_j} = 2.7 \left(\frac{d}{x} \right)^{\frac{1}{2}}, \quad \ell = 0.078x \quad (32)$$

where

$$\int_{-\infty}^{+\infty} U^2 dy = U_j^2 d \quad (33)$$



Thermal Plumes

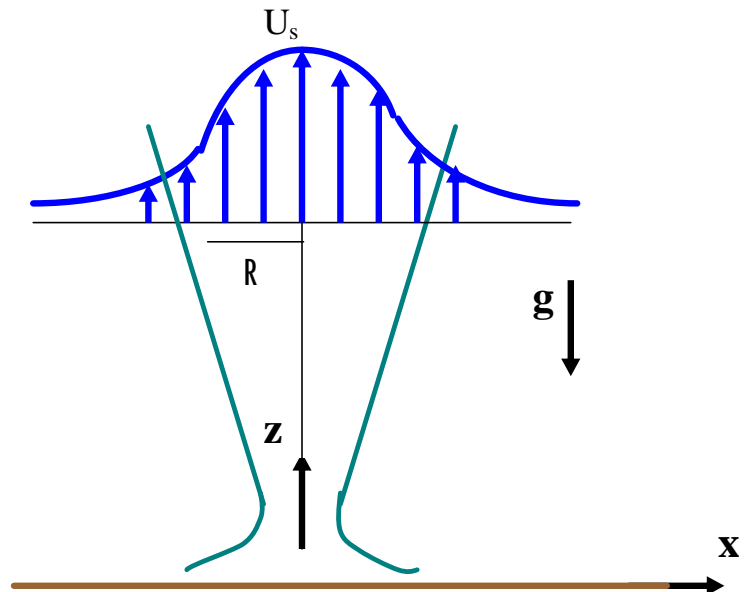
The equations governing the motion and heat transfer turbulent flows are given as

$$\left\{ \begin{array}{l} U_j \frac{\partial U_i}{\partial x_j} + \frac{\partial}{\partial x_j} \overline{u'_i u'_j} = -\frac{1}{\rho} \frac{\partial P}{\partial x_i} + \nu \frac{\partial^2 U_i}{\partial x_j \partial x_j} + \frac{g_0 \bar{T}}{T_0} \delta_{ij}, \quad \frac{\partial U_i}{\partial x_i} = 0 \\ U_j \frac{\partial \bar{T}}{\partial x_j} + \frac{\partial}{\partial x_j} \overline{T' u'_j} = \gamma \frac{\partial^2 \bar{T}}{\partial x_j \partial x_j} \end{array} \right. \quad (1)$$

The special case of two-dimensional thermal plumes is described in the following section.

Two Dimensional Plane Plumes

For a two a two-dimensional plume as shown in the figure, the equation of balance of moment, heat flow and continuity are given as:



$$U \frac{\partial W}{\partial x} + W \frac{\partial W}{\partial z} + \frac{\partial}{\partial x} \overline{u' w'} = \frac{g_0 \bar{T}}{T_0} \quad (2)$$

$$U \frac{\partial \bar{T}}{\partial x} + W \frac{\partial \bar{T}}{\partial z} + \frac{\partial}{\partial x} \overline{T' u'} = 0 \quad (3)$$

$$\frac{\partial U}{\partial x} + \frac{\partial W}{\partial z} = 0 \quad (4)$$

In addition the heat flux integral given by

$$\int_{-\infty}^{+\infty} \overline{T} W dx = \text{const} = \frac{q}{\rho c_p} \quad (5)$$

Introducing the similarity variables

$$\mathbf{x} = \frac{x}{\ell} \quad (6)$$

the following self similar solutions may be assumed:

$$W = U_s f(\xi), \quad -\overline{u'w'} = U_s^2 g(\xi), \quad \overline{T} = T_s \theta(\xi), \quad -\overline{T'u'} = T_s U_s h(\xi) \quad (7)$$

Now let

$$U_s = Az^m, \quad \ell = Bz^n, \quad T_s = cz^p \quad (8)$$

Equation (2) implies that

$$2m - 1 = 2m - n = p \quad \text{or} \quad n = 1 \quad \text{and} \quad p = 2m - 1 \quad (9)$$

Equation (5) implies that

$$m + p + n = 0 \quad \text{or} \quad m + p = -1 \quad (10)$$

Equations (9) and (10) imply that

$$m = 0 \quad \text{and} \quad p = -1. \quad (11)$$

Hence,

$$U_s = \text{const}, \quad \ell = Bz, \quad T_s = Cz^{-1}. \quad (12)$$

Now

$$\xi = \frac{x}{\ell} = \frac{x}{Bz}, \quad \frac{\partial \xi}{\partial x} = \frac{1}{Bz}, \quad \frac{\partial \xi}{\partial z} = -\frac{\xi}{z} \quad (13)$$

Introducing the stream function

$$\psi = \ell U_s F(\xi), \quad F' = f, \quad \psi = U_s Bz F(\xi) \quad (14)$$

$$W = U_s F', \quad U = -\frac{\partial \psi}{\partial z} = -U_s B(F - \xi F'), \quad \frac{\partial W}{\partial x} = \frac{U_s}{Bz} F'' \quad (15)$$

$$\frac{\partial W}{\partial z} = -\frac{U_s \xi}{z} F'', \quad T = Cz^{-1} \theta(\xi), \quad \frac{\partial T}{\partial x} = Cz^{-2} \theta', \quad \frac{\partial T}{\partial z} = -Cz^{-2} (\theta + \xi \theta'), \quad (16)$$

$$-\frac{\partial \overline{u'w'}}{\partial x} = \frac{U_s^2}{Bz} g', \quad -\frac{\partial \overline{T'u'}}{\partial x} = \frac{U_s C}{B} z^{-2} h'. \quad (17)$$

Using (14)-(17) in (2) and (3), we find

$$-U_s B(F - \xi F') \frac{U_s}{Bz} F'' + U_s F' \left(-\frac{U_s \xi}{z} \right) F'' = \frac{U_s^2}{Bz} g' + \frac{g_0 C}{T_0 z} \theta \quad (18)$$

$$-U_s B(F - \xi F') \frac{C}{B} z^{-2} \theta' + U_s F' (-cz^{-2}) (\theta + \xi \theta') = \frac{U_s C}{B} z^{-2} h' \quad (19)$$

Simplifying Equations (18) and (19), we find

$$-FF'' = \frac{1}{B} g' + \frac{g_0 C}{T_0 U_s^2} \theta \quad (20)$$

$$-(F\theta)' = \frac{1}{B} h' \quad (21)$$

Introducing the eddy viscosity,

$$\nu_T = \frac{-\overline{u'w'}}{\frac{\partial W}{\partial x}} = -\frac{\overline{\theta'u'}}{\frac{\partial T}{\partial x}} = U_s \ell \frac{g}{F''} = U_s \ell \frac{h}{\theta'} \quad (22)$$

or

$$g = \frac{1}{R_T} F'', \quad h = \frac{1}{R_T} \theta' \quad (23)$$

Now letting

$$B = \frac{1}{R_T} \text{ and } \frac{g_0 C}{T_0 U_s^2} = 1 \quad (24)$$

Then

$$FF'' + F''' + q = 0 \quad (25)$$

$$F\theta + \theta' = \text{const} = 0 \quad (26)$$

The corresponding boundary conditions are:

$$F'(0) = 1, \quad F(0) = 0, \quad F'(\infty) = 0, \quad \theta(0) = 1, \quad (27)$$

An exact solution is not available. Here an approximate solution is presented. In the neighborhood of $x = 0$,

$$F \approx \xi + \dots \quad (28)$$

It then follows that

$$\frac{\theta'}{\theta} = -\xi, \quad \ln \theta \approx -\frac{\xi^2}{2} + \ln c, \quad \theta \approx e^{-\frac{\xi^2}{2}} \quad (29)$$

Equation (25) may then be approximated as

$$F''' + \xi F'' = -e^{-\frac{\xi^2}{2}}, \quad (30)$$

The solution to (30) is

$$F'' = -\xi e^{-\frac{\xi^2}{2}} \quad (31)$$

Integrating (30), it follows that

$$f = F' = e^{-\frac{\xi^2}{2}} \quad (32)$$

Therefore, the mean velocity and temperature fields in the plume are given by

$$\frac{W}{U_s} = e^{-\frac{\xi^2}{2}}, \quad \frac{T}{T_s} = e^{-\frac{\xi^2}{2}}. \quad (33)$$