

Incompressible Viscous Flows

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Navier-Stokes Equation

Continuity

$$\nabla \cdot \mathbf{v} = 0$$

Navier-Stokes

$$\frac{\partial \mathbf{v}}{\partial t} + \mathbf{v} \cdot \nabla \mathbf{v} = -\frac{1}{\rho} \nabla P + \nu \nabla^2 \mathbf{v}$$

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Outline

- Navier-Stokes Equation
- Steady Parallel Flows
- Boundary Conditions
- Unsteady Parallel Flow
- Boundary Layer Flows
- Flow over a Flat Plate
- Blasius Solution
- Laminar Boundary Layer

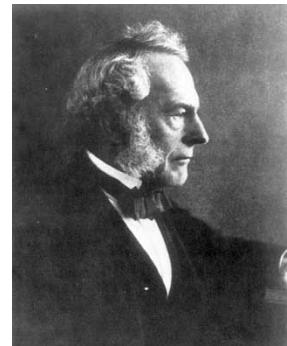
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Navier-Stokes Equation



Navier



Stokes

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Navier-Stokes Equation

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Incompressible Fluid

$$\begin{aligned}\rho\left(\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z}\right) &= \rho g_x - \frac{\partial p}{\partial x} + \mu\left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2}\right) \\ \rho\left(\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z}\right) &= \rho g_y - \frac{\partial p}{\partial y} + \mu\left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2}\right) \\ \rho\left(\frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z}\right) &= \rho g_z - \frac{\partial p}{\partial z} + \mu\left(\frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2}\right)\end{aligned}$$

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

4 Equations for 4
unknowns u, v, w and p

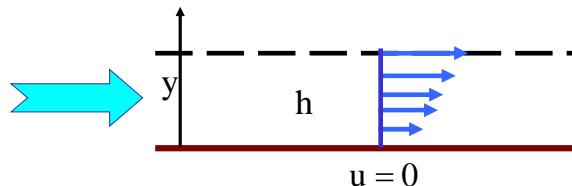
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Steady Parallel Flows

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Cartesian Coordinates



$$u(y), v = 0, w = 0$$

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Steady Parallel Flows

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Cartesian Coordinates

$$\rho g_x - \frac{\partial p}{\partial x} + \mu \frac{d^2 u}{dy^2} = 0$$

General Solution

$$u = -\frac{1}{2\mu} \left(\rho g_x - \frac{\partial p}{\partial x} \right) y^2 + A y + B$$

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Boundary Conditions

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Solid Walls

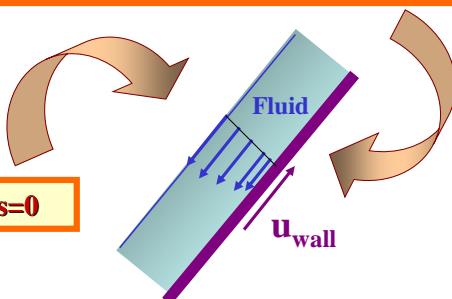
A viscous fluid sticks to its boundary, $u_{fluid} = u_{wall}$

Free Surface

Shear Stress=0

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Boundary Conditions

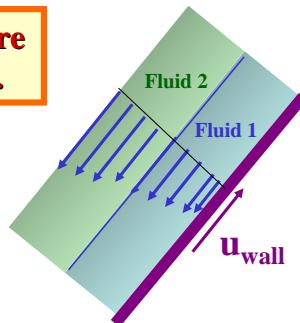
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Between Two Fluids

Velocity and shear stress are the same at the interface.

$$u_1 = u_2$$

$$\tau_1 = \tau_2$$



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Steady Parallel Flows

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Cartesian

$$\rho g_x - \frac{\partial p}{\partial x} + \mu \frac{d^2 u}{dy^2} = 0$$

$$u = -\frac{1}{2\mu}(\rho g_x - \frac{\partial p}{\partial x})y^2 + Ay + B$$

Cylindrical Axial

$$\rho g_z - \frac{\partial p}{\partial z} + \mu \frac{1}{r} \frac{d}{dr} (r \frac{dv_z}{dr}) = 0$$

$$v_z = -\frac{1}{4\mu}(\rho g_x - \frac{\partial p}{\partial z})r^2 + A \ln r + B$$

Rotating

$$\frac{d^2 v_\theta}{dr^2} + \frac{1}{r} \frac{dv_\theta}{dr} - \frac{v_\theta}{r^2} = 0$$

$$v_\theta = Ar + \frac{B}{r}$$

$$\frac{dp}{dr} = \rho \frac{v_\theta^2}{r}$$

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Plate Suddenly Set in Motion

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$$\frac{\partial u}{\partial t} = v \frac{\partial^2 u}{\partial y^2}$$

B.C.

$$y = 0$$

$$u = U_0$$

y

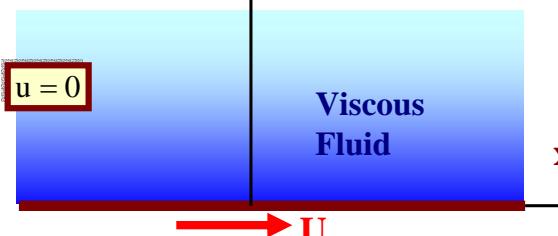
$$y = \infty$$

$$u = 0$$

I.C.

$$t = 0$$

$$u = 0$$



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Plate Suddenly Set in Motion

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Similarity Solution

Let

$$t \sim t^1$$

$$y \sim t^a$$

Navier-Stokes

$$1 = 2a$$

$$a = 1/2$$

Similarity Variables

$$\eta = \frac{y}{2\sqrt{vt}}$$

$$\frac{u}{U_0} = f(\eta)$$

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Plate Suddenly Set in Motion

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$$\text{NS} \rightarrow f'' + 2\eta f' = 0$$

$$\rightarrow f' = ce^{-\eta^2}$$

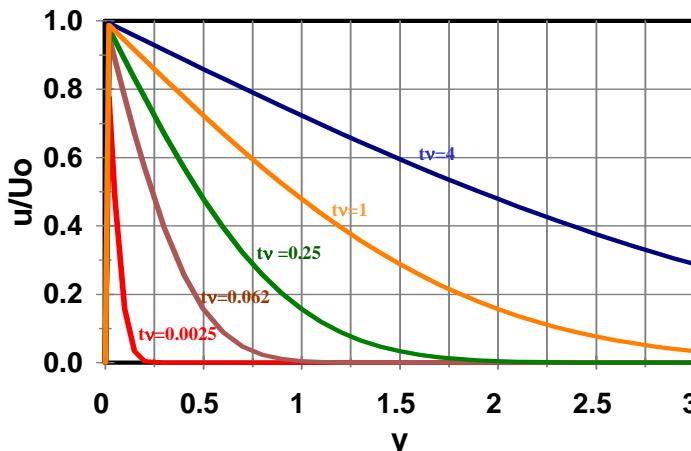
$$f = 1 - \frac{2}{\sqrt{\pi}} \int_0^\eta e^{-\eta_1^2} d\eta_1 = 1 - \text{erf}(\eta)$$

Solution

$$u = U_0 \text{erfc}\left(\frac{y}{2\sqrt{vt}}\right)$$

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Variation of velocity profile with time.

Boundary Layer

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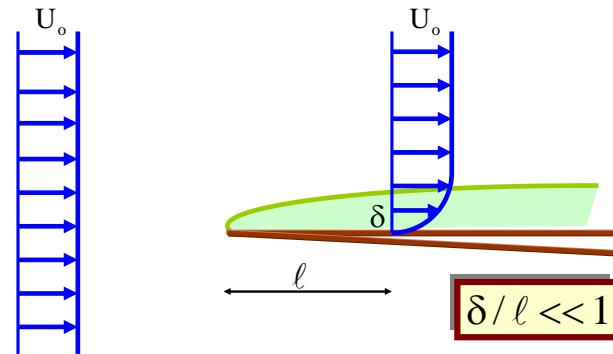


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Boundary Layer over a Flat Plate

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Laminar Boundary Layer

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Boundary Layer Thickness

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Boundary Layer Thickness, δ

Distance at which

$$\frac{u}{U_0} = 0.99$$

Displacement Thickness

Distance at which

$$\delta^* = \int_0^\infty \left(1 - \frac{u}{U_0}\right) dy$$

Momentum Thickness

Distance at which

$$\theta = \int_0^\infty \frac{u}{U_0} \left(1 - \frac{u}{U_0}\right) dy$$

Shape Factor

Distance at which

$$H = \frac{\delta^*}{\theta}$$

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Boundary Layer Theory

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Steady Two-D Flows

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + v \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right)$$

$$u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial y} + v \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right)$$

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

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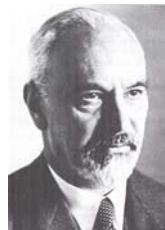
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Boundary Layer Equations

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$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho} \frac{dp}{dx} + v \frac{\partial^2 u}{\partial y^2}$$

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$



Ludwig Prandtl

Boundary Conditions

Distance at which

$$\text{at } y = 0 \quad u = 0, v = 0$$

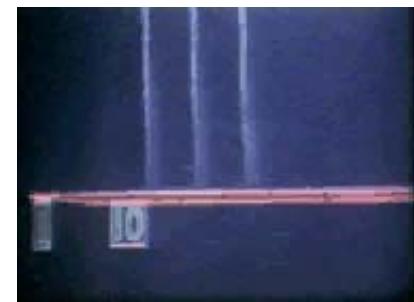
$$\text{at } y = \infty \quad u = U_0$$

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Boundary Layer over a Flat Plate

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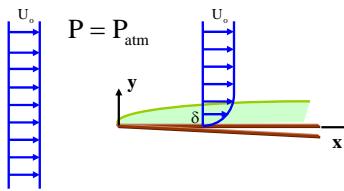
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Boundary Layer over a Flat Plate

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$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = v \frac{\partial^2 u}{\partial y^2}$$



$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

Boundary Conditions

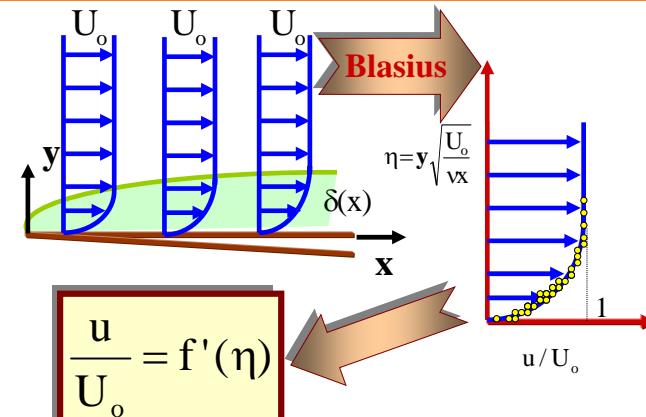
at $y = 0$ $u = 0, v = 0$
at $y = \infty$ $u = U_o$

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Blasius Solution

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Blasius Similarity Solution

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$$\eta = y \sqrt{\frac{U_o}{vx}}$$

$$\frac{u}{U_o} = f'(\eta)$$

$$\frac{\partial u}{\partial y} = f''(\eta) \sqrt{\frac{U_o}{vx}}$$

Blasius Equation

Boundary Layer Eq.

Boundary Conditions

$$ff'' + 2f''' = 0$$

at $\eta = 0$ $f = 0, f' = 0$
at $\eta = \infty$ $f' = 1$

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Blasius Similarity Solution

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Boundary Layer Thickness, δ

$$\delta = 5 \sqrt{\frac{vx}{U_o}}$$

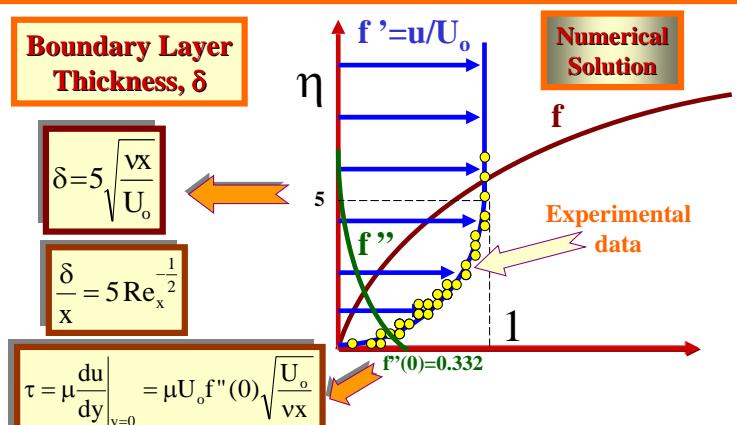
$$\delta = 5 Re_x^{-\frac{1}{2}}$$

$$\tau = \mu \left. \frac{du}{dy} \right|_{y=0} = \mu U_o f''(0) \sqrt{\frac{U_o}{vx}}$$

Numerical Solution

Experimental data

1



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Boundary Layer over a Flat Plate

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Friction Coefficient

$$C_F = \frac{\tau}{\frac{1}{2} \rho U_o^2} = \frac{2f''(0)}{\sqrt{R_{ex}}} = \frac{0.664}{\sqrt{R_{ex}}}$$

Drag Coefficient

$$C_D = \frac{D}{\frac{1}{2} \rho U_o^2 \ell} = \frac{4f''(0)}{\sqrt{R_{el}}} = \frac{1.328}{\sqrt{R_{el}}}$$

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Summary

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Boundary Layer over a Flat Plate

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Displacement Thickness

$$\delta^* = \int_0^\infty \left(1 - \frac{U}{U_0}\right) dy = 1.721 \sqrt{\frac{vx}{U_0}}$$

Momentum Thickness

$$\theta = \int_0^\infty \frac{U}{U_0} \left(1 - \frac{U}{U_0}\right) dy = 0.664 \sqrt{\frac{vx}{U_0}}$$

Shape Factor

$$H = \frac{\delta^*}{\theta} = 2.51$$

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Thank you!

Questions?

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