



ME 326 - Intermediate Fluid Mechanics 

Turbulent Boundary Layer

Goodarz Ahmadi
 Department of Mechanical and Aeronautical Engineering
 Clarkson University
 Potsdam, NY 13699-5725


ME 326 G. Ahmadi

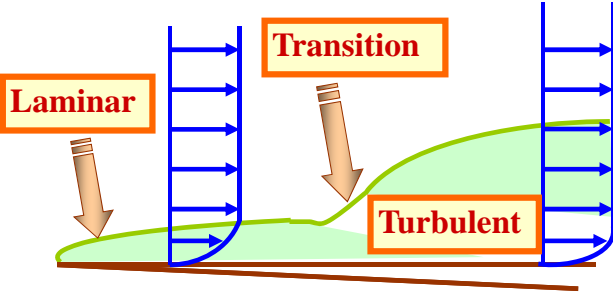
Turbulent Boundary Layer 

Outline


- Transition
- Turbulent Boundary Layer Flows
- Momentum Integral Method
- Drag on Smooth Plates
- Drag on Rough Plates
- Empirical Equations for Drag

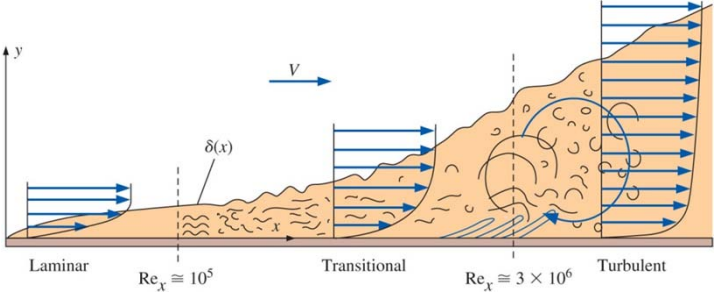
ME 326 G. Ahmadi

Boundary Layer Transition 



ME 326 G. Ahmadi

Boundary Layer Transition 



ME 326 G. Ahmadi

Boundary Layer over a Flat Plate Clarkson University

Boundary Layer Thickness

→

$\frac{\delta}{x} = 5 \text{Re}_x^{-\frac{1}{2}}$

Laminar

Friction Coefficient
 $C_D = 1.328 \text{Re}_\ell^{-\frac{1}{2}}$

$\text{Re}_\ell = \frac{U_0 \ell}{\nu}$

Critical Reynolds Number


→

$\text{Re}_{\text{crit}} \approx \begin{cases} 3.2 \times 10^5 \sim 10^6 \\ 5 \times 10^5 \sim 3 \times 10^6 \end{cases}$

ME 326 G. Ahmadi

Reynolds' Experiments

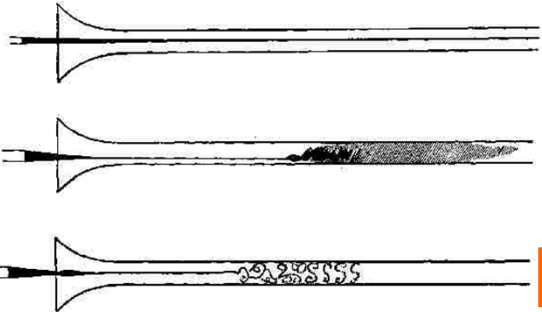
Reynolds Pipe Flow Experiment



ME 326 G. Ahmadi

Reynolds' Experiments

Reynolds Pipe Flow Experiment



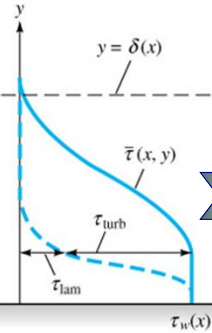
Laminar

Turbulent

Transition

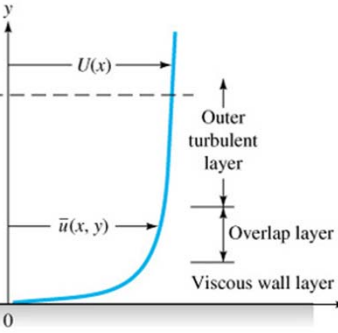
ME 326 G. Ahmadi

Turbulent Velocity Profiles Clarkson University



(a)

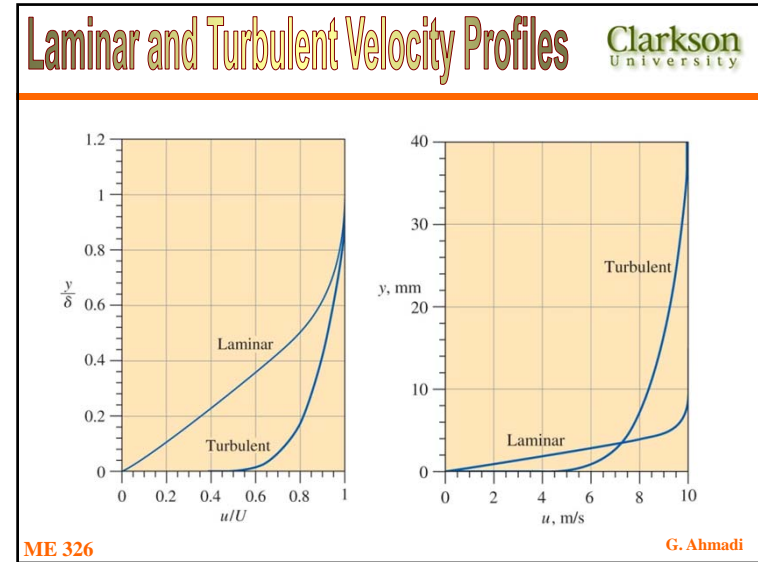
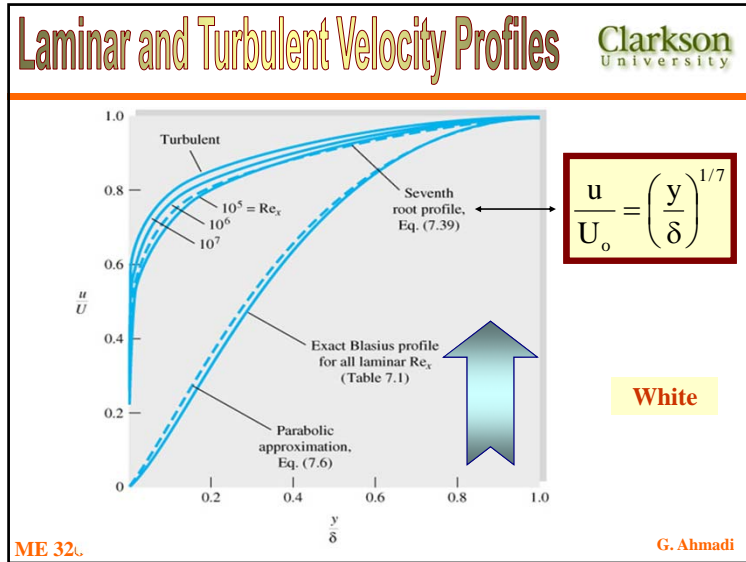
→



(b)

White

ME 326 G. Ahmadi



Inertial Sublayer

Clarkson University

Turbulent Stress=Wall Shear Stress

$$\tau_0 = \rho \kappa^2 y^2 \left(\frac{\partial u}{\partial y}\right)^2 \implies \frac{du}{dy} = \frac{u^*}{\kappa y} \quad u^* = \sqrt{\frac{\tau_0}{\rho}}$$

$$\frac{u}{u^*} = u^+ = \frac{1}{\kappa} \ln y + c$$

Wall Units

$$u^+ = \frac{1}{\kappa} \ln y^+ + B$$

$$y^+ = \frac{u^* y}{\nu}$$

$B \approx 5$

$30 < y^+ \leq 300$

ME 326 G. Ahmadi

Viscous Sublayer

Clarkson University

Turbulent stress is negligible $0 < y^+ \leq 5$

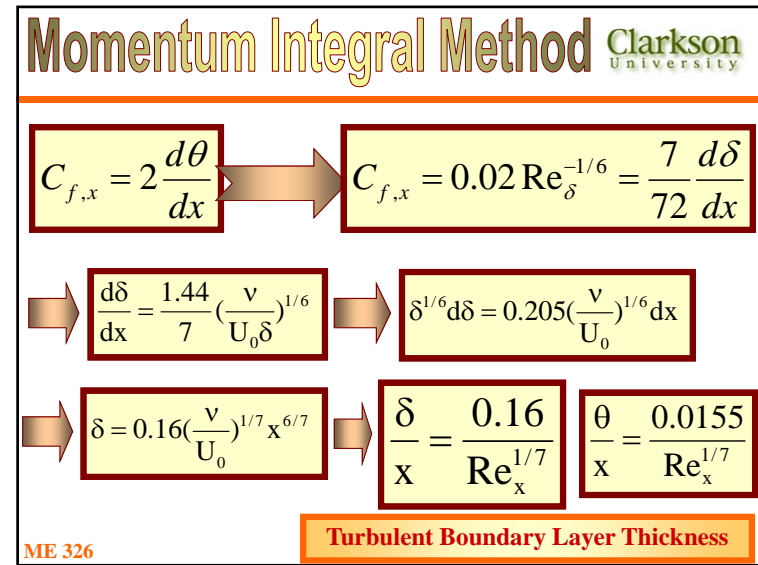
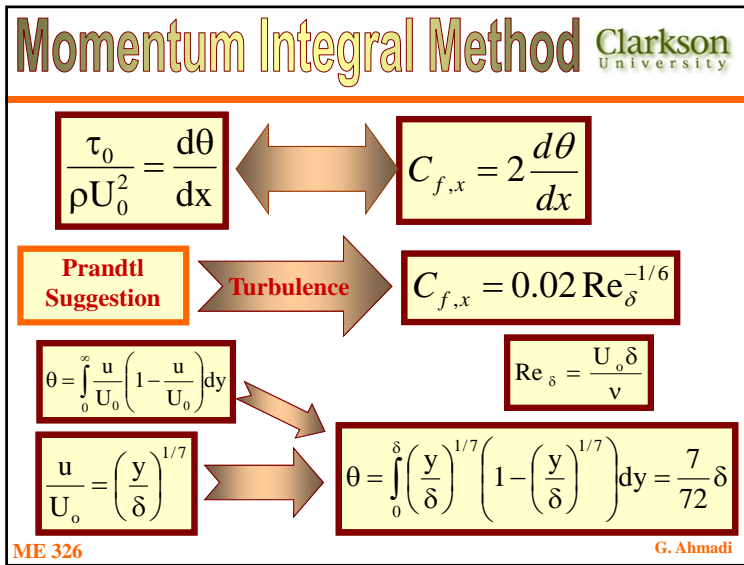
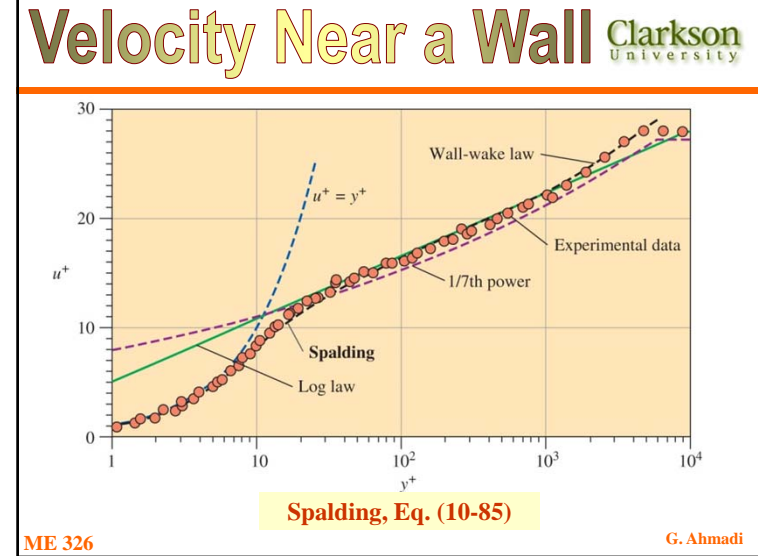
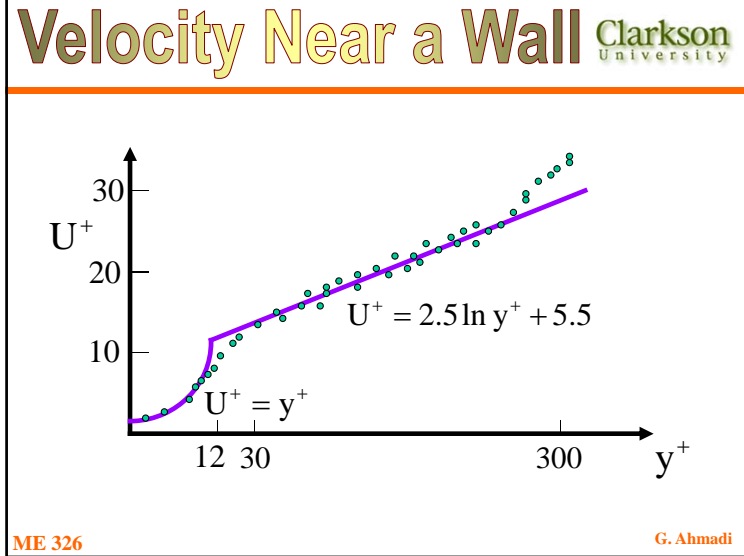
$$\tau_0 = \mu \frac{du}{dy}$$

$$u^{*2} = \nu \frac{du}{dy}$$

$$\frac{du^+}{dy^+} = 1$$

$$u^+ = y^+$$

ME 326 G. Ahmadi



Turbulent Boundary Layer - Smooth Clarkson University

$\frac{\delta}{x} = \frac{0.16}{\text{Re}_x^{1/7}}$

$\delta^* = \frac{1}{8} \delta$

$H = \frac{\delta^*}{\theta} = 1.3$

Friction Coefficient

➔

$C_{f,x} = 2 \frac{d\theta}{dx} = \frac{0.027}{\text{Re}_x^{1/7}}$

Drag Coefficient

➔

$C_D = 2 \frac{\theta(L)}{L} = \frac{0.031}{\text{Re}_L^{1/7}}$

ME 326G. Ahmadi

Transition Clarkson University

Schlichting Equations

$C_D = \frac{0.031}{\text{Re}_L^{1/7}} - \frac{1440}{\text{Re}_L} \quad \text{Re}_{\text{Trans}} = 5 \times 10^5$

$C_D = \frac{0.031}{\text{Re}_L^{1/7}} - \frac{8700}{\text{Re}_L} \quad \text{Re}_{\text{Trans}} = 3 \times 10^6$

ME 326G. Ahmadi

Average Friction Coefficient Clarkson University

Laminar

$C_D = \frac{1.326}{\text{Re}_L^{1/2}} \quad \text{Re}_L \leq 5 \times 10^5$

Turbulent

$C_D = \frac{0.074}{\text{Re}_L^{1/5}} \quad 5 \times 10^5 \leq \text{Re}_L \leq 10^7$

Corrected for laminar part

$C_D = \frac{0.074}{\text{Re}_L^{1/5}} - \frac{1742}{\text{Re}_L} \quad 5 \times 10^5 \leq \text{Re}_L \leq 10^7$

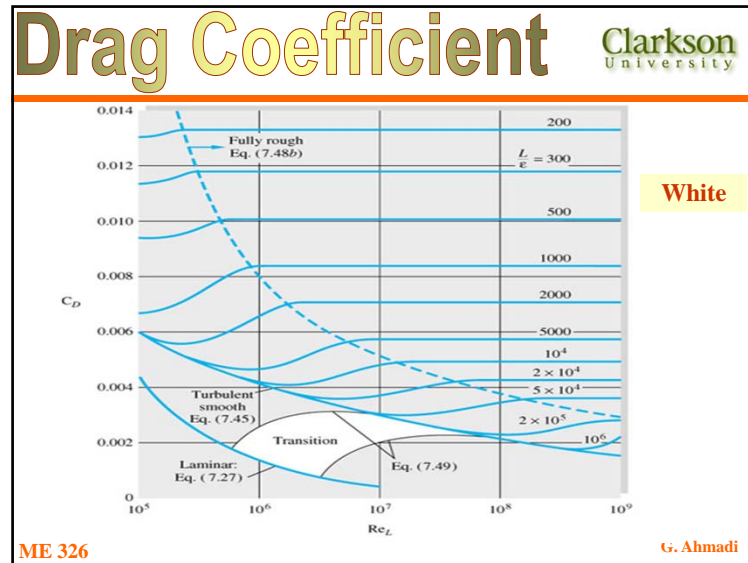
ME 326G. Ahmadi

Rough Walls Clarkson University

$C_F = \left(2.87 + 1.58 \log \frac{x}{\epsilon} \right)^{-2.5}$

$C_D = \left(1.89 + 1.62 \log \frac{L}{\epsilon} \right)^{-2.5}$

ME 326G. Ahmadi



Turbulent Boundary Layer

Clarkson University

Concluding Remarks

- Transition
- Turbulent Boundary Layer Flows
- Momentum Integral Method
- Drag on Smooth Plates
- Drag on Rough Plates
- Empirical Equations for Drag

ME 326

G. Ahmadi

Clarkson University

Thank you!

Questions?

ME 326

G. Ahmadi